PROPOSED SYSTEMS IN VIEW OF APPLICATIONS

	System Id	Salt	Solvent	Solute	Investigated propertiy(ies)	Application
	1 a				VLE (solubilities, vaporization of	Gas storage, Distillation, active ingredient
Only fluid		NRS		НС	neutral cpds)	manufacturing
Phase Eq	1b	NRS	Protic	НС	LLE (Solute partitioning)	Extraction, purification
	1 c	NRS	Aprotic	НС	LLE (Solute partitioning)	Extraction, purification
	2a	NRS		AG	VLE (solubilities)	Gas storage /
	2b					gas scrubbing / absorption/
Fluid Phase +	20	RSB		AG	VLE (solutes partitioning)	geothermal
reaction	2c	RSA		BG	VLE (solutes partitioning)	gas scrubbing / absorption
reaction	2d	OrgS	Protic		VLE (all volatiles partitioning)	Separation / stripping
	2e	OrgS	Aprotic		VLE (all volatiles partitioning)	separation
	2f	RSB	Protic		VLE (vaporization of neutral cpds)	Evaporation (distillation)
	3a				ELS (solid appearance condition and	
Solid Phase no	Ja	NRS			amount)	salt purification; water treatment
reaction in the	3b	NRS		HC	ELS (solid appearance condition)	scaling - flow assurance
	3c	NRS	Protic		ELS (solid appearance condition)	scaling - flow assurance
liquid phase	3d	NRS		НС	ELS (solid appearance condition and	<u>crystallisation of active compounds</u> ;
	Su	INNO		ПС	amount)	<u>flow assurance</u>
Solid phase +	4a	OrgS			Activities, speciation	<u>Batteries</u>
reaction	4b	MOx			ELS, speciation (pH)	Corrosion, catalyst manufacturing



NRS

New energy technologies require the capacity to store large amount of gases. This may [| | be natural gas or increasingly hydrogen. It may also be a mixture of hydrogen and methane (hythane).

A very efficient large scale solution is to store these gases in salt caverns that contain an aquifer. This aquifer is a brine, most often containing NaCl.

The solubility of the gas to be stored must be determined, as well as the water content of the gas.

Challenge: Pressure conditions are generally high, and very few data exist with high ionic strength water.

				Temperatur	e
salt	co-solvent	solute	Property	range	Pressure range
NaCl; CaCl ₂	none	H ₂ ; CH ₄	Ki (VLE) (gas; water)	up to 200 °C	200 bar
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In geothermal applications, water is recovered in temperature conditions that may be EleTher supercritical. In these conditions, salts are soluble in molecular form. When temperature is lowered, new types of vapour-liquid equilibrium can appear, where ions appear in both liquid and vapour phases

Challenge: (1) **Data**: measuring VLE and SLE in high temperature conditions may be a real challenge; (2) most of today's **models** consider that the ionic species remain in the liquid phase. This is no longer true in conditions where water has a very low dielectric constant.

				Temperatu	re
salt	co-solvent	solute	Property	range	Pressure range
NaCl; CaCl2; CaCO3			Ki (VLE) (gas solubility; solvent vaporization)	550 °C	up to 500bar





RSB



In gas treatment technologies, a solvent is used for removing reactive gases. Chemical solvents are much more efficient as they allow a higher solubility of the gas in the solvent, but regeneration issues may then become important (heat needed to recover the gas from the solvent).

AG

Challenge: Many different types of reacting salts can be used, including organic salts, for which very few data exist.

The enthalpy of reaction and vaporization of the gas is a key piece of information in these processes, since it determines the global energy efficiency.

The loss of solvent through vaporization is often badly studied. This vaporization strongly depends on the speciation in the aqueous phase.

salt	co-solvent	solute	Property	Temperatur range	e Pressure range
amine salts; NaOH; K0	OH Amine	CO ₂ ; H ₂ S; SO _x ; NO _x	Ki (VLE) (gas solubility; solvent vaporization); enthalpies	140 °C	up to 100 bar
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The objective of extraction processes is to ensure that a solute passes from one liquid phase to another. One of the liquid phases is often aqueous.

HC

HC

Example:

Liquid-liquid extraction is used in the fuel cycle to separate fission products from Uranium and Plutonium.

Challenges: Most of the operations take place at 20-40 °C but for specific safety studies, extrapolation of data are needed from 40 to 100-120 °C leading to major uncertainties.

			Temperatui	re
co-solvent	solute	Property	range	Pressure range
HNO _{3,} Tributyl Phosphate; C12 alkane		Ki(VLLE)	20-120 °C	around 1 atm
	HNO _{3,} Tributyl Phosphate;	HNO _{3,} Tributyl Phosphate;	HNO _{3,} Tributyl Phosphate;	co-solvent solute Property range HNO3, Tributyl Phosphate; Ki(VLLE) 20-120 °C





Stripping occurs when a inert gas is used to remove unwanted components from an aqueous phase.



Example:

Alcohols and acids are removed from a fermentor that contains alcohol, water, organic acids and a pH buffer (typically NaOH, KOH or NH₃OH). The volatility of the compounds strongly depends on the pH as a consequence of the speciation of the acid.

Challenge: data exist for some acids; often determined at low concentrations (pKa). No data exist for higher molecular weight acids. In addition, when the concentration is large, non-idealities need to be considered in the liquid phase which means that a model needs to be used. No data exists for these high molecular weight material.

salt	co-solvent	solute	Property	Temperatu range	re Pressure range
NaOH; KOH; NH₃OH	alcohols (ethanol, propanol)	organic acids	Ki (VLE) (solute; water)	50 °C	1-2 bar





NRS

VLE (solubilities, vaporization of neutral cpds)

Gas storage, distillation



Alkali hydroxides are commonly used during batch reaction steps for the production of active ingredients. NaCl as well as complex polyatomic salts, like phenolates, can be formed as intermediates. The reaction mixture is further processed, requiring e.g. a distillation (batch or continuous) for a solvent exchange or the distillative separation of residual water. For this purpose, in particular knowledge on the VLE of the solvents as well as the solubility of the salts in different solvent mixtures is of interest.

Challenge: The large variety of possible compounds will necessitate some predictive approach (group contribution method or other kind of property – structure relationships) to extrapolate the data

				Temperatu	re
salt	co-solvent	solute	Property	range	Pressure range
e.g. Phenolates, NaCl, NaOH, KOH	Various organic solvents (alcohols, ethers, acetonitrile	nhenolates	VLE, SLE		10 - 1013 mbar
© 2016 FPEN	DMAC, etc.)		Contact: thomas.gerla	ich1@bayer.com	Energies nouvelles

HC

ELS (solid appearance condition and amount)

crystallisation of active
compounds; flow assurance



Apart from the process design, in the development phase of new active ingredients, the solubility of complex polyatomic molecules in different buffer and salt solutions is required. These information are of interest in particular in an early development phase, requiring highly predictive models. Depending on the pH, the API might exist in different ionized forms.

Challenge: The large variety of possible compounds will necessitate some predictive approach (group contribution method or other kind of property – structure relationships) to extrapolate the data

				Temperature		
salt	co-solvent	solute	Property	range	Pressure range	

NaCl, buffer solutions

API

Solubility of API (SLE)

1 bar



3d

NRS

HC.

ELS (solid appearance condition and amount)

crystallisation of active compounds; flow assurance

Formation water typically contains a wealth of ions, which could lead to precipitation of salts at suitable conditions and/or upon mixing with aqueous streams of different compositions. It is important to be able to use limited available data for simple systems and conditions away from those of interest, to develop models that can predict the behaviour of more complex systems and their blending. Common ion effects, effect of ratio of anion/cation, differences with respect to ion valence, are thought to be crucial for the behaviour of these systems.

Challenge: How would BaSO₄ or SrSO₄ behave at different ratios of the ions, different conditions, and at the presence of CaCO₃? How does Total Dissolved Solids affect the model? Can we increase confidence on how we transfer knowledge from simple systems to more complex ones?

				Temperatur		
salt	co-solvent	solute	Property	range	Pressure range	
Ba, Sr, Ca /SO₄; CO₃	Possibly with alcohols		SLE	40-150 °C	up to 400 bar, with a few applications reaching up to 1000 bar	
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4a

OrgS

Activities, speciation

Batteries



Batteries require a high energy intensity, meaning a high content of ionic species. Yet, in aqueous media, the voltage is limited by the decomposition voltage of water. As a consequence, there is an active search for electrolytic media based on organic species, that still dissolve as ions in water. The redox potentials of these products are needed, hence the formation properties and the ionic activity coefficients. Examples are quinones in water. How can we increase confidence on the prediction of dielectric constant for such systems?

Challenge: Very few data exist for (1) solubility; (2) speciation; (3) activity coefficients and (4) formation properties of these organic salts. Everything needs to be done.

Temperature salt co-solvent solute Property range Pressure range

Organic salts (benzoquinones)

ionic activity; solubility (SLE); speciation





4b MOx

ELS, speciation (pH)

Corrosion, catalyst manufacturing



Corrosion is essentially a redox chemical reaction between a solid and a liquid. This means that the species activity as well as their crystallization tendency must be modeled simultaneously.

Challenge: Few data exist in extreme conditions (e.g. high CO₂ or H₂S pressures, or in the presence of impurities that may affect the reaction -dissolved oxygen).

salt	co-solvent	solute	Property	Temperature range	e Pressure range
FeO; FeO ₂ ;			ionic activity; solubilit (SLE); speciation	y 20 – 150 °C	Up to 200 bar





4b

MOx

ELS, speciation (pH)

Corrosion, catalyst manufacturing



Catalyst manufacturing is based on the deposition of well-controlled metallic oxides on a support. In order to make sure that the correct oxide is being deposited, it is essential to control precisely the speciation in liquid phase as a function of pH and temperature condition.

Challenge: Considering the high concentrations, an adequate model must be available to describe non-idealities, in addition to reactive equilibrium. Several solid phases may co-exist, and making sure that the correct one is deposited is a challenge.

				Temperature	
salt	co-solvent	solute	Property	range	Pressure range

MnO; Ni(OH); NaClO₄; NiCO₃; Ni(NO₃)₂; Ni(HCO₃); HP(Mo_xO_v)

ionic activity; solubility (SLE) ; 20 – 80 °C speciation

Atm.



NUCLEAR WASTE TREATMENT

The High Liquid Level Waste Concentration collects and concentrates the high liquid wastes whigh contain most of the activity of the fuel. Due to the number of elements in the liquid solution, speciation is a big challenge that could help to achieve a better management of the corrosion of the boiler and to understand the development of fouling which results in reduced thermal capacity. In addition a chemical reaction between HCOH and HNO₃ producing NO_x takes place in the boiler.

Challenge: No tool exists capable to describe the large amount of reactions that occur in high concentrated solution.

salt	co-solvent	solute	Property	Temperat range	ure Pressure range
Fission Products (Cs, Po Ru, Tc, Zr)	u, H₂O/HNO₃	NOx, H₂CO	solubility (SLE) ; speciation	100-120°C	1 bar





SALT PRODUCTION



Pure salt products are often obtained as a solid that precipitates as a result of a chemical reaction. However, many reactants may coexist in the aqueous phase, and it is essential that the correct solid is precipitated.

Industrial example:

- Precipitated Calcium Carbonate (PCC) is a high value product that can be recovered from marble wastes. It is produced by adding CO2 to a CaO rich aqueous solution.

Challenge: Several solid phases can precipitate. In order to model this correctly, there is a need to parameterize both the aqueous phase thermodynamic up to high salt concentration, and the solid phase(s) formation properties. Both have an impact on the results. Only limited data is available.

salt	co-solvent	solute	Property	range	Pressure range
CaCO3; CaO		CO2	solubility (SLE) ; speciation	??	??



